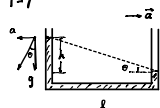


7-7



在管的非惯性系下, 等势面与水面向大角 θ , $\tan\theta = \frac{a}{g}$

故由几何关系 $h = l \tan\theta = \frac{a}{g} l$

7-10 取包含 A, B 的流管, 忽略 A, B 高度差 $\frac{1}{2}\rho v_A^2 + P_A = \frac{1}{2}\rho v_B^2 + P_B$ 其中 $P_B = P_0$

由连续性, 流量 $Q = S_A \cdot v_A = S_B \cdot v_B$

A 处吸起 h 水柱 $P_0 - P_A = \rho g h$

由上述各式得 $h = \frac{Q^2}{2g} \left(\frac{1}{S_A^2} - \frac{1}{S_B^2} \right)$

7-13 (1) 水柱高为 h, 对水的质元 m: $\frac{1}{2}m v^2 = m g H \Rightarrow$ 出口速度: $v = \sqrt{2gH}$

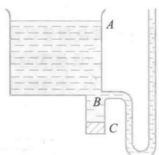
体积流量: $Q = \frac{1}{4}\pi d^2 \cdot v = \frac{1}{4}\pi d^2 \sqrt{2gH}$

(2) 取喷嘴流管 $\frac{1}{2}\rho v_0^2 + P = \frac{1}{2}\rho v^2 + \rho g h + P_0$

连续性 $Q = \frac{1}{4}\pi D^2 \cdot v_0 \Rightarrow v_0 = \frac{D^2}{d^2} \sqrt{2gH}$

由上述各式得 $P = P_0 + \rho g \left[h + H \left(1 - \frac{d^4}{D^4} \right) \right]$

7-14



题 7-14 图

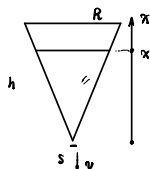
(1) 连通器: $h_1 = h_A$

(2) 取包含 A, B, C 的流管 $\rho g h_A + P_0 = \rho g h_B + \frac{1}{2}\rho v^2 + P_B = \rho g h_C + \frac{1}{2}\rho v^2 + P_0$

B 处示数 h_2 $P_B = P_0 + \rho g (h_2 - h_B)$

由上述各式得 $h_2 = h_C$

7-17



取从水面到孔流管 (S 为小孔, $\frac{1}{2} \leq x \leq h$, 故忽略水面移动速度)

$\rho g x + P_0 = \frac{1}{2}\rho v^2 + P_0 \Rightarrow v = \sqrt{2gx}$

流量 $Q = S \cdot v = S \sqrt{2gx}$

$Q = \frac{dV}{dt} = -\frac{\pi R^2}{h^2} x^2 \frac{dx}{dt}$

故 $t = -\frac{\pi R^2}{S h^2} \frac{1}{\sqrt{2g}} \int_h^{\frac{h}{2}} x^{\frac{3}{2}} dx = \frac{\pi R^2}{20S} \sqrt{\frac{h}{g}} (4\sqrt{2} - 1)$

7-18 (1) 取小段, 由泊肃叶公式 $Q = \frac{\pi R^4 dP}{8\eta dl}$ 其中 $dP = \rho g dl$

$$\text{故 } \eta = \frac{\pi \rho g R^4}{8Q}$$

$$\omega \text{ 管轴处: } v_0 = \frac{R^2 dp}{4\eta dl} = \frac{2Q}{\pi R^2}$$

$$7-20 \text{ 斯托克斯公式 } f = 6\pi\eta r v_r$$

$$\text{总力 } f = \rho g \frac{4}{3}\pi r^3$$

$$\text{故 } v_r = \frac{2\rho g r^2}{9\eta} = 1.425 \times 10^{-2} \text{ m/s}$$

7-23

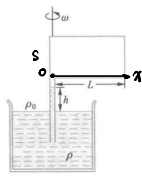


图 7-23 图

考虑等温状态下压强的玻尔兹曼分布 $\frac{P}{P} = \text{Const} = \frac{P_0}{P_0}$

对一小段空气 $SdP = \rho S \pi \omega^2 dx$

$$\Rightarrow \rho_0 \omega^2 \pi dx = \rho_0 \frac{dP}{P}$$

$$\text{积分 } P = P_1 e^{\frac{\rho_0 \omega^2 \pi^2}{2P_0}} \quad \text{其中 } P_1 \text{ 为 } x=0 \text{ 处的压强}$$

$$\rho = \rho_1 e^{\frac{\rho_0 \omega^2 \pi^2}{2P_0}} \quad \rho_1 \text{ 为 } x=0 \text{ 处的密度}$$

$$\text{归一化, 总质量 } m = \rho_0 S L = \int_0^L \rho S dx = \rho_1 S \int_0^L e^{\frac{\rho_0 \omega^2 \pi^2}{2P_0}} dx$$

$$\Rightarrow P_1 = P_0 \cdot \frac{L}{\int_0^L e^{\frac{\rho_0 \omega^2 \pi^2}{2P_0}} dx}, \quad \rho_1 = P_0 \cdot \frac{L}{\int_0^L e^{\frac{\rho_0 \omega^2 \pi^2}{2P_0}} dx}$$

$$\omega \text{ 很小, } \frac{\rho_0 \omega^2 \pi^2}{2P_0} \ll 1, \text{ 做近似 } \int_0^L e^{\frac{\rho_0 \omega^2 \pi^2}{2P_0}} dx \approx \int_0^L \left(1 + \frac{\rho_0 \omega^2 \pi^2}{2P_0} x\right) dx = L \left(1 + \frac{\rho_0 \omega^2 \pi^2 L}{6P_0}\right)$$

$$P_1 \approx P_0 \cdot \frac{1}{1 + \frac{\rho_0 \omega^2 \pi^2 L}{6P_0}} \approx P_0 - \frac{1}{6} \rho_0 \omega^2 L^2$$

$$\text{吸起 } h \text{ 水柱 } \rho g h = P_0 - P_1 = \frac{1}{6} \rho_0 \omega^2 L^2$$

$$\text{得 } h = \frac{\rho_0 \omega^2 L^2}{6\rho g}$$